# **Optimizing Bioreactor Landfills: Biogas Production and Nitrogen Biotransformation**

### Introduction

As the American public becomes more aware of the current energy crisis, the search for sufficient quantities of renewable energy to offset current fossil fuel utilization and keep pace with increasing energy demand is ever growing. Sustainable renewable energy cannot be obtained from a single source; a combination of sources such as wind, solar, hydroelectric, geothermal and biomass will be needed.

Municipal solid waste (MSW) naturally decomposes to produce carbon dioxide (CO2) and methane (CH4), a fuel gas, and bioreactor landfill technology (Figure 1) can be employed to enhance waste degradation and biogas recovery. Thus, MSW should be viewed as a fuel, and solid waste management systems should be optimized to maximize biogas generation (through the stimulation of methanogens) and collection, while minimizing energy demands. A dynamic energy balance for Burlington County's (New Jersey, USA) bioreactor landfill was developed to quantify the potential energy recovery from landfill biogas versus the energy consumed during regular landfill management (Equation 1).

Some of the energy consumed comes from the need to treat heavily ammonia-loaded leachate and ship it to a wastewater treatment facility for disposal. Classical methods for treating ammonia-rich leachate include stimulating nitrification followed by denitrification in various types of reactors, chemical precipitation, nanofiltration, and air stripping [3]. These methods are very costly and must be done ex-situ.

A newly discovered anaerobic ammonium oxidation (ANAMMOX) pathway (Equation 2) has been described in wastewater treatment plants as well as marine sediments [4-7] and research is currently underway for finding anammox capable species in a bioreactor landfill system [2]. Unlike methanogenesis where there are several archeal species capable of producing methane, there are only 4 known deeply branching Planctomycetales capable of catalyzing anammox [4-7]. In a bioreactor landfill system, it is likely to be easier to stimulate methanogenesis than anammox, however ammonia treatment is a large cost for the landfills and should be dealt with in the most efficient manner; currently, this involves stimulating anammox as well as methanogens within the same system.

Table 1

## **Energy Balance for the Bioreactor Landfill**



 $\frac{dE_{net}}{dE} = E_{biogas} - r$  $-E_{transport(ir)}$ 

### Equation 1 – The Dynamic Energy Balance

•  $dE_{net}/dt$  = Net system energy for a specified time interval •  $E_{biogas}$  = Potential recoverable energy from landfill biogas • *Etransport(in)* = Energy necessary to transport MSW and landfill cover from a point of origin to the landfill •  $E_{transport(out)}$  = Energy necessary to transport leachate and stormwater from the bioreactor landfill to wastewater treatment

facilities

• *E*<sub>operation</sub> = Energy utilized to construct and maintain the bioreactor landfill and supporting infrastructure

The boundaries of the energy balance are broadly defined to include MSW, cover material and leachate transport as well as landfill operations. Actual data was utilized in all possible circumstances. Assumptions with respect to vehicle fuel economy were made based on sample average



D. Babson, and J. Loudon, Department of Environmental Sciences, Rutgers University, New Brunswick, NJ Pollution and Environmental Microbiology, Spring 2007

### **Nitrogen Transformation**

 $NH_4 + 1.26NO_2^- + 0.085CO_2 + 0.02H^+ \rightarrow N_2 + 0.017H^+ + 0.24NO_3^- + 1.95H_2O_2^-$ Equation 2 - Anammox uses ammonium as the electron donor and nitrite as the electron acceptor in a ratio of approximately 1:1. Change in Gibbs free energy is -357 kJ/rk.



Figure 3 - Potential pathways of nitrogen transformation and/or removal in bioreactor landfills [3].

Parameter	Nitrification NH <sub>4</sub> <sup>+</sup> + $O_2 \rightarrow NO_2^-$	Anammox NH $_{4}^{+}$ + NO $_{2}^{-} \rightarrow N_{2}$	Unit
Free energy	-275	-357	kJ/mol
Biomass yield	0.08	0.07	mol/mol C
Aerobic rate	200–600	0	nmol/min/ mg proteir
Anaerobic rate	2	60	nmol/min/ mg proteir
Growth rate	0.04	0.003	/h
Doubling time	0.73	10.6	days
$K_{s} NH_{4}^{+}$	5-2600	5	μM
K <sub>s</sub> NO₂ <sup>−</sup>	N/A	<5	μM
K <sub>s</sub> O <sub>2</sub>	10–50	N/A	μM

 
 Table 1 - aerobic vs. anaerobic
ammonia oxidation [8]

### The Dynamic Energy Balance

$$(E_{transport(out)} - E_{operation})$$



specified waste management system

reference (BTU/gallon of diesel).





# **Microbial Community**

As seen by denaturing gradient gel electrophoresis (DGGE), the microbial community within landfill leachate is very complex (Fig.4). Among the diversity, we have distinguished several species of methanogens as well as nitrifiers and denitrifiers. Anammox species are patchy and much harder to find within a given leachate collection site. We are still confident that conditions within the bioreactor landfill system are favorable for anammox species, and further investigation is being done.

It is interesting to note that while methanogens seem to be more widely distributed than anammox species, the process of methanogenesis is much more energetically unfavorable compared to nitrogen utilization by anammox species

### Optimization

Carbon Source + hydrogen source  $\rightarrow$  methane + hydrogen

Ex. CO2 + 4H2 → CH4 + 2H2O

Equation 3 - Basic methanogenesis equation (change in Gibbs free energy is -131 kJ/rk)

At bioreactor landfills where energy from biogas is being generated, maximum methane production may be desirable, however, if the goal is also to minimize the waste management's carbon footprint or other environmental impacts, there can be numerous tradeoffs.

When attempting to minimize the carbon footprint of the waste management system, the system energy balance needs to be maximized. A tradeoff of this may be utilizing the bioreactor to lower nitrogen species in-situ by stimulating anammox. Since there is competition between the various microbial communities for available electron donor (hydrogen), anammox processes may limit methanogenesis. More study is needed to delineate such links, and to asses the extent and value of using the bioreactor to pre-treat leachate.

### References

1. Babson, D. 2007. Unpublished Data.

2. Loudon, J. 2007. Unpublished Data.

3. Berge, ND., DR. Reinhart, and TG Townsend. 2005. The Fate of Nitrogen in Bioreactor Landfills. Critical Reviews in Envrionmental Science and Technology. 35:365-399.

4. Pynaert, K., BF. Smets, S. Wyffels, D. Beheydt, SD. Siciliano, and W. Verstraete. 2003. Characterization of an Autotrophic Nitrogen-Removing Biofilm from a Highly Loaded Lab-Scale Rotating Biological Contactor. Applied and Environmental Microbiology. 69:3626-3635.

5. Tal, Y., JEM. Watts, and HJ. Schreier. 2005. Anaerobic Ammonia-Oxidizing Bacteria and Related Activity in Baltimore Inner Harbor Sediment. Applied and Envrionmental *Microbiology.* 71:1816-1821.

6. Egli, K., U. Fanger, PJJ. Alavarez, H. Siegrist, JR. van der Meer, and AJB Zehnder. 2001. Enrichment and Characterization of an Anammox Bacterium from a Rotating Biological Contactor Treating Ammonium-Rich Leachate. Archives of Microbiology. 175:198-207

7. Schmid, M., K. Walsh, R. Webb, WI. Rijpstra, K. van de Pas-Schoonen, MJ. Verbruggen, T. Hill, B. Moffett, J. Fuerst, S. Schouten, JS. Damste, J. Harris, P. Shaw, M. Jetten, and M. Strous. 2003. Candidatus "Scalidua brodae" sp.nov., Candidatus "Scalindua wagneri" sp.nov., two new species of anaerobic ammonium oxidizing bacteria. Systems in Applied Microbiology. 26:529-538

8. Jetten, MSM., M. Wagner, J. Fuerst, M. van Loosdecht, G. Kuenen, and M. Strous. 2001. Microbiology and Application of the Anaerobic Ammonium Oxidation Process. Current Opinion in Biotechnology. 12:283-288.



